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# Anions, Complexing and Salting - Out Agents Effects on the Extraction of Cr (VI) from HCI and H<sub>2</sub>SO<sub>4</sub> Acid Media Using Chloroform Solution of Bis (4-acylpyrazolones)

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# Authors' contributions

This research work was carried out between the authors in the department of pure and industrial chemistry, University of Port Harcourt. Author BAU designed the project which was carried out by author IAK as part of her Ph.D research works on Cr (VI) extraction studies. The analysis and interpretation of results were performed by both authors. Both authors read and approved the final manuscript.

## Article Information

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# ABSTRACT

Extraction of Cr(VI) into chloroform solutions of 4-adipoylbis (1- phenyl-3methypyrazolone-5), H<sub>2</sub>Adp and 4-sebacoylbis (1- phenyl-3-methypyrazolone-5), H<sub>2</sub>SP were carried out and the effect of the anions, Cl<sup>-</sup>, SO<sub>4</sub><sup>2-</sup>, Br<sup>-</sup>, l<sup>-</sup>, SCN<sup>-</sup>, PO<sub>4</sub><sup>2-</sup>, EDTA, Oxalate acetate and tartarate were studied. The results showed that the masking effect of the halides on the extraction of Cr(VI) followed theorder l<sup>-</sup> <Br<sup>-</sup><Cl<sup>-</sup>. This is consistent with the order of increase in electronegactivity of the element and decrease in ionic radius of the ions. The effect of complexing agents such as, PO<sub>4</sub><sup>2-</sup>, acetate EDTA, oxalate and tartarate on the extraction of Cr (VI) ions appears to be fairly constant for both H<sub>2</sub>Adp and H<sub>2</sub>SP. The results obtained show that extractions of these metals are increasingly masked as

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anion concentration increase in the aqueous phase. The extraction of the metal is reduced in the presence of salting-out agent using  $H_2Adp$ . Better extractions were obtained when  $H_2SP$  was used as the extractant. This shows that  $H_2SP$  is a better extractant than  $H_2Adp$  for Cr (VI).

Keywords: Complexing agents; extractant; chloroform; salting – out agents; masking agents; butanol.

### **1. INTRODUCTION**

The  $\beta$  diketones, 4-adipoylbis(1-phenyl-3methylpyrazolone-5), (H<sub>2</sub>Adp) and 4sebacoylbis(1-phenyl-3-methylpyrazolone-5).

( $H_2SP$ ) were synthesized for the first time and characterized [1]. They have been found to exhibit the ability of effectively trapping toxic metals such as Fe, Cd, Cu, Ni, Mn, U, V and W from water. This is the main reason for their proposed use in organic solutions as [2,3,4]. Studies have shown that 4-acylpyrazolones are efficient extractants forming stable complexes with some group I, II and transition metals [1,5,6,7,8,9]. Liquid –liquid extraction of uranium (VI) and vanadium (V) ions using these chelating agents have been studied and reported [10,11,12].

Several methods have been used for the extraction of Cr (VI). Among these methods are the use of methyl isobutyl ketone (MIBK) [13], triisoctylamine (TIOA) [14] and other methods for the determination of the Cr (VI), [15,16]. The extraction of chromium (VI) in acidic chloride media using tributyl phosphate (TBP) has been [17]. reported The neutral extractant. triphenylphosphin (TPP) has been reported to be an efficient complexing agent for the transport of Cr (VI) from sulphuric acid solutions. The extracted species is the (HTPP) HCr<sub>2</sub>O<sub>7</sub> complex [18]. The research is aimed at studying the effect of the anions, complexing and salting-out agents have on the extraction of Cr (VI). The degree of extraction of Cr (VI) in various concentrations of Cl<sup>-</sup> and SO<sub>4</sub><sup>2-</sup> in the presence and absence of HCl and H<sub>2</sub>SO<sub>4</sub> respectively will be studied.

#### 2. MATERIALS AND METHODS

#### 2.1 Preparation of Stock Solutions

#### 2.1.1 Preparation of chromium stock solution

A stock solution of Cr (VI) was prepared by dissolving 0.0373 g of potassium chromate,  $(K_2CrO_4)$  in a small volume of 0.001M HCl in a 100cm<sup>3</sup> volumetric flask and made up to mark with the 0.001M HCl solution. The working solutions were prepared by diluting appropriate

volumes of the stock solution with an appropriate volume of water in a  $10 \text{ cm}^3$  volumetric flasks.

#### 2.1.2 Preparation of organic stock solutions

Fresh solutions of the organic extraction reagents, 4-adipoyl-bis (1-phenyl-3-methylpyrazolones-5)  $H_2Adp$  and 4-sebacoyl-bis (1-phenyl-3-methylpyrazolones-5)  $H_2SP$  were prepared as and when required. Appropriate weights of the extractants were dissolved in CHCl<sub>3</sub> to obtain the concentration of the working organic reagent of 0.01M. These solutions ( $H_2Adp$  and  $H_2SP$ ) were stable for at least a month.

#### 2.1.2.1 4-adipoylbis(1-phenyl-3methylpyrazolone-5) H<sub>2</sub>Adp

The standard solution of this extraction reagent was prepared by dissolving 0.4585 g of H<sub>2</sub>Adp in a small volume of CHCl<sub>3</sub> in a 100 cm<sup>3</sup> volumetric flask and made up to mark with CHCl<sub>3</sub>. The concentration of the resultant solution was 0.01M H<sub>2</sub>Adp/CHCl<sub>3</sub> (stock solution). Working solutions were prepared by diluting appropriate volumes of this stock solution with CHCl<sub>3</sub>.

#### 2.1.2.2 4-sebacoylbis(1-phenyl-3methylpyrazolone-5) H<sub>2</sub>SP

The standard solution of this extraction reagent was prepared by dissolving 0.5146 g of  $H_2SP$  in small volume of CHCl<sub>3</sub> in a 100 cm<sup>3</sup> volumetric flask and made up to mark with CHCl<sub>3</sub>. The concentration of the resultant solution was 0.0IM  $H_2SP/CHCl_3$  stock solution. Working solutions were prepared by diluting appropriate volumes of this stock solution with CHCl<sub>3</sub>

#### 2.1.3 Preparation of salting – out agents

The salting – out agents were prepared as and when required. The working solutions were prepared by diluting the stock solutions with appropriate volumes of deionized water.

# 2.1.4 Preparation of solutions of complexing agents

Fresh stock solutions of the complexing agents were always prepared when needed. Working

solutions were prepared by taking suitable volumes of the stock and diluting with deionized water.

#### **2.2 Extraction Procedures**

#### 2.2.1 Extraction in the presence of complexing agents

A 0.2 ml volume of the metal ion solution was introduced into 10 extraction bottles. A solution of a complexing agent was added into these bottles. Water was subsequently added to each of the bottles to adjust the volume of the aqueous phase to 1ml so that the final dilution gave solutions with the following range of concentrations of the anions:

Br- ions :	0.001M -	2M
SCN- ions:	0.001M -	1M
Acetate ions:	0.001M -	1M
PO₄ <sup>3-</sup> ions:	0.001M -	1M
$C_2O_4^{2-}$ ions:	0.001M -	0.08M
Tartrate ions:	0.001M -	0.08M
EDTA ions:	0.001M -	0.08M

Equal volume  $(1 \text{ cm}^3)$  of the 0.01M H<sub>2</sub>Adp (or H<sub>2</sub>SP) solution was added to each extraction bottle and agitated for 30 minutes. The phases were allowed to settle and separated and the unextracted metal ions in the aqueous phase determined. These processes were also carried out with the CHCl<sub>3</sub>/BuOH mixture.

#### 2.2.2 Extraction in the presence of saltingout agents

A 0.2 ml aliquot of the metal ion solution was pipetted into 10 extraction bottles. Into these bottles, solutions of the salting-out agent and mineral acid were added. Water was added to adjust the volume of the aqueous phase to 1cm<sup>3</sup> such that the final dilution gave a concentration range of the salting – out agents as follows:

NH₄CI:	0.001M -	4M
Na <sub>2</sub> SO <sub>4</sub> :	0.001M -	1M

In the presence of the mineral acids, a specific volume (0.1 ml) and concentration of the acid having a common anion with the salting out agent in the extraction bottle was used. Hence, each of the extraction bottles contained any of the following combinations:  $NH_4CI/HCI$  and  $Na_2SO_4/H_2SO_4$  with Cr(VI) in the aqueous phase.

#### 2.2.3 Extraction in the presence of a synergist

An equal volume of chloroform solution of the 0.01M  $H_2Adp$  (or  $H_2SP$ ) was agitated with the aqueous solution in the extraction bottles for 30 minutes. The phases were allowed to settle and were separated. The amount of Cr (VI) in the aqueous raffinate was analysed.

Butanol was added as the synergist. The extractants ( $H_2Adp$  and  $H_2SP$ ) were prepared according to the procedure outlined earlier, using a CHCl<sub>3</sub>/BuOH mixture in the ratio of 4:1. The resultant solution was a 0.01M standard solution of the extractants. The standard solutions were used for all levels of investigation.

#### 2.2.4 Determination of Cr (VI)

Chromium (VI) ions present in the aqueous raffinate were determined using diphenylcarbazide (DPC) [19,20]. A 0.5 cm<sup>3</sup> volume of the Cr (VI) extraction raffinate was introduced into 5cm<sup>3</sup> sample bottles. A 0.5cm<sup>3</sup> volume of 10M H<sub>2</sub>SO<sub>4</sub> was added followed by 1cm<sup>3</sup> of DPC forming a violet complex. The mixture was made up to 5cm<sup>3</sup> with deionized water. The absorbance of the complex was obtained at 540nm and the amount of Cr (VI) in the aqueous solution after extraction was determined using the absorbance of the solution from a standard calibration curve.

For each set of results, new calibration curves were obtained at the same time that the chromium ions in the extraction raffinate were analysed.

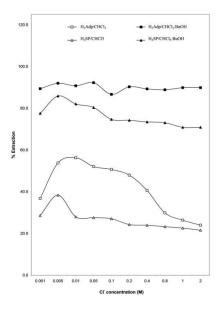
### 3. RESULTS AND DISCUSSION

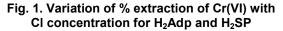
# 3.1 Effect of the Anions on the Extraction of Cr (VI)

Fig. 1 shows that at concentration of Cl<sup>-</sup> ions less than 0.01M, the % extraction of Cr (VI) appears to be independent of Cl<sup>-</sup> ion concentration in the aqueous phase. At this concentration, about 52% of Cr (VI) was extracted using H<sub>2</sub>Adp compared to 28% extraction by H<sub>2</sub>SP which is an indication that H<sub>2</sub>Adp is a better extractant for Cr (VI) in the presence of Cl<sup>-</sup> ions. When BuOH was added to the organic phase, the % extraction increased tremendously to an average of 90% and 80% for H<sub>2</sub>Adp and H<sub>2</sub>SP respectively. The result also shows that the extraction of Cr (VI) into BuOH solution of the ligands in chloroform is independent of Cl<sup>-</sup> ion concentration. The effect of  $SO_4^{2^-}$  ion is presented in Fig. 2. For H<sub>2</sub>Adp, the % extraction appears to be fairly constant between 60% and 65% but for H<sub>2</sub>SP, it is observed that the % extraction tend to increase with increase in  $SO_4^{2^-}$  concentration. Hence the % extraction increased from 30% at 0.001M  $SO_4^{2^-}$  to 86% at 1M  $SO_4^{2^-}$  concentration. It is apparent that  $SO_4^{2^-}$  ions have a tremendous salting – out effect on the H<sub>2</sub>SP complex with Cr (VI) but not with the H<sub>2</sub>Adp complex. Addition of BuOH into the organic phase resulted in an increase in the % extraction of Cr (VI) from solutions containing  $SO_4^{2^-}$  ions by both ligands.

#### 3.1.1 The effect of thiocyanide ions

The effect of SCN<sup>-</sup> is presented in Fig. 3. The synergistic effect of BuOH is observed for both ligands. The results obtained show that the % extraction of Cr (VI) by both ligands appears to be fairly constant throughout the range of SCN<sup>-</sup> concentrations studied.

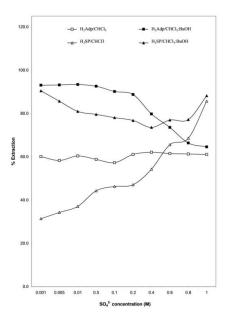




#### 3.1.2 The effect of Br and I ions

The effect of Br and I ions on the extraction process is presented in Fig. 4. This is similar to what was observed for extraction from CI ion solution presented in Fig. 1. The % extraction appears to be fairly constant throughout the concentrations studied. However, it is pertinent to note that extraction is more efficient by both ligands when the solution contains iodide ions

than when it contains bromide ions. This is an indication that the Br<sup>-</sup> ion has a higher masking effect than the iodide ion. At 0.1M concentration of halide ions for instance, 60% extraction of Cr(VI) from Br<sup>-</sup> solution byH<sub>2</sub>Adp was achieved while 86% extraction from iodide ion solution was obtained. It appears that the smaller ionic radius of Br<sup>-</sup> ion may have been responsible for this masking effect since it could more easily interact with the metal ion to form unextractable metal bromo complexes.



# Fig. 2. Variation of % extraction of Cr(VI) with $SO_4^{2^2}$ concentration for H<sub>2</sub>Adp and H<sub>2</sub>SP

A comparism of the three halides studied shows that the masking effect of these halides is in an increasing order as follows:

I<sup>-</sup><Br<sup>-</sup><Cl<sup>-</sup>forH<sub>2</sub>Adp

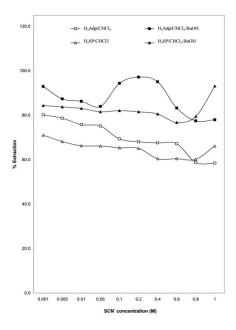
The trend in this case is consistent with the order of increase in electronegativity of the element and decrease in ionic radius of the ions.

#### 3.2 Effect of Complexing Agent

#### 3.2.1 Effect of phosphate and acetate ions

The effect of  $PO_4^{2-}$  ions and acetate ions is illustrated in Fig. 5. Apart from the % extraction of Cr (VI) with H<sub>2</sub>Adp from solutions of  $PO_4^{2-}$  ion which appears to decrease gradually, increase in both acetate and  $PO_4^{2-}$  ion concentrations

appears to cause a decrease in the % extraction of Cr (VI) ions by both ligands. Hence, the masking effects of the anions tend to increase slightly with increase in anion concentration in the aqueous phase for both ligands.



#### Fig. 3. Variation of % extraction of Cr (VI) with SCN concentration for H<sub>2</sub>Adp and H<sub>2</sub>Sp

#### 3.2.2 Effect of EDTA

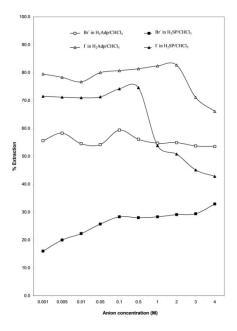
Fig. 6 shows that the % extraction is fairly constant as the concentration of EDTA increases from 0.01M to 1M. Synergism is observed when BuOH is introduced into the organic phase. The effect is more pronounced in the extraction with  $H_2Adp$  where the % extraction increased from 30% to 92%.

#### 3.2.3 Effect of oxalate and tartrate

The effect of oxalate ion presented (Fig. 7.) appears to be similar to that of EDTA. The % extraction of Cr (VI) remained fairly constant throughout the concentration range of the complexing agent studied. The only exception however, is the extraction with  $H_2Adp$ . Beyond 0.01M oxidation concentration, there appears to be a monotonous decrease in the amount of Cr (VI) extracted even in the presence of BuOH as a synergist.

Fig. 8 shows that the % extraction of Cr (VI) tends to decrease slightly as the concentration of tartarate ion increased. This is observed for both

H<sub>2</sub>Adp and H<sub>2</sub>SP even with BuOH as a synergist. Fig. 8 shows that synergism of BuOH is more pronounced for extraction with H<sub>2</sub>Adp than with H<sub>2</sub>SP. This is because with H<sub>2</sub>Adp, the % extraction increased from 43% to 86% at 0.001M tartrate ion concentration whereas with H<sub>2</sub>SP the increment was from 62% to 78% at the same tartrate ion concentration.



#### Fig. 4. Variation of % extraction of Cr (VI) with anion concentration for H<sub>2</sub>Adp and H<sub>2</sub>Sp

#### 3.3 Salting-out Effect of Acid Anions in Acid Solution

The salting-out effect of Cl<sup>-</sup>and SO<sub>4</sub><sup>2-</sup> ions on the extraction of Cr (VI) from HCl and H<sub>2</sub>SO<sub>4</sub> solutions respectively is depicted in Figs. 9 to 16. Figs. 9 to 12.show the effect of the acidic anions (Cl<sup>-</sup> and SO<sub>4</sub><sup>2-</sup>) on the % extraction of the metal from its acid solution using H<sub>2</sub>Adp. It shows that rather than acting as a salting – out agent, the acid in solution reduces the % extraction of Cr (VI) which is at variance with what was reported for Mo (VI), [21].

The % extraction is reduced by 5% to 20% for both anions in the presence of their respective acids. Even the addition of BuOH did not change the pattern of the extraction process.

The result obtained using H<sub>2</sub>SP as extractant is presented in Figs. 13 to 16 showing that both Cl<sup>-</sup> and SO<sub>4</sub><sup>2-</sup> anions have some salting-out effect on the extraction of Cr(VI) from the acid species solutions similar to that of Mo(VI). This shows,

that H<sub>2</sub>SP is a better extractant than H<sub>2</sub>Adp when these anions are used as salting-out agents.

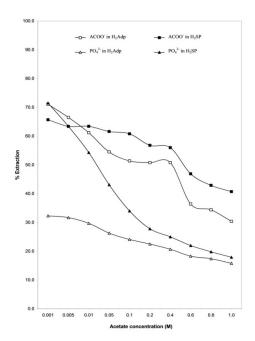
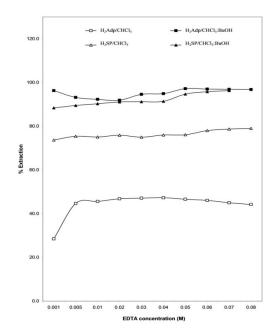
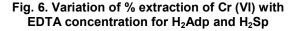


Fig. 5. Variation of % extraction of Cr (VI) with anion concentration for  $H_2Adp$  and  $H_2Sp$ 





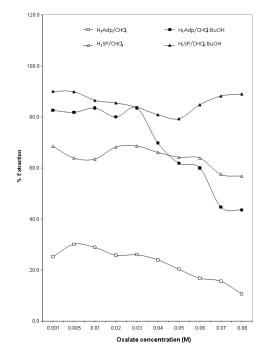


Fig. 7. Variation of % extraction of Cr (VI) with oxalate concentration for H<sub>2</sub>Adp and H<sub>2</sub>Sp

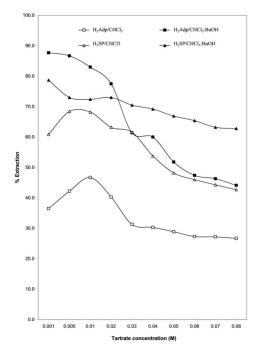


Fig. 8. Variation of % extraction of Cr (VI) with tartrate concentration for H<sup>2</sup>Adp and H<sub>2</sub>Sp

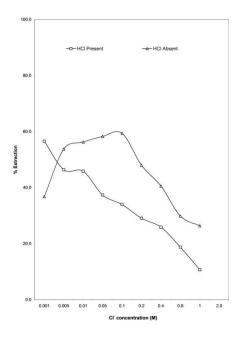


Fig. 9. Variation of % extraction of Cr (VI) with CI concentration for H<sub>2</sub>Adp in CHCl<sub>3</sub>(in the presence and absence of HCI)

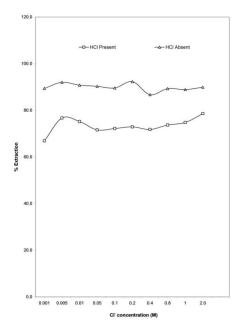


Fig. 10. Variation of % extraction of Cr (VI) with Cl concentration for H<sub>2</sub>Adp in CHCl<sub>3</sub>:BuOH(in the presence and absence of HCl)

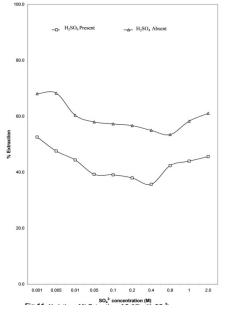


Fig. 11. Variation of % extraction of Cr (VI) with  $SO_4^{2^\circ}$  concentration for H<sub>2</sub>Adp in CHCI<sub>3</sub>:BuOH(in the presence and absence of H<sub>2</sub>SO<sub>4</sub>)

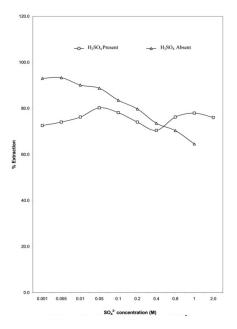


Fig. 12. Variation of % extraction of Cr (VI) with SO<sub>4</sub><sup>2-</sup> concentration for H<sub>2</sub>Adp inCHCI<sub>3</sub>:BuOH(in the presence and absence of H<sub>2</sub>SO<sub>4</sub>)

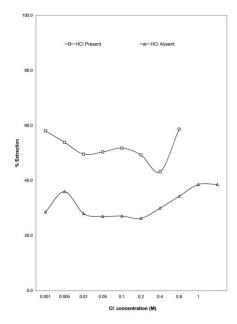


Fig. 13. Variation of % extraction of Cr (VI) with CI concentration for H<sub>2</sub>Adp in CHCI<sub>3</sub>(in the presence and absence of HCI)

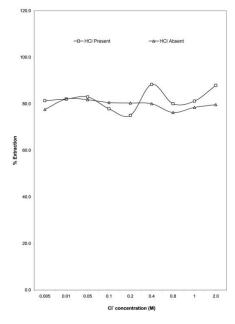


Fig. 14. Variation of % extraction of Cr (VI) with Cl concentration for H<sub>2</sub>SP in CHCl<sub>3</sub>:BuOH(in the presence and absence of HCl)

## 4. CONCLUSION

The decrease in metal ion extraction with increase in  $Cl^{-}$  and  $SO_{4}^{2-}$  ion concentration has

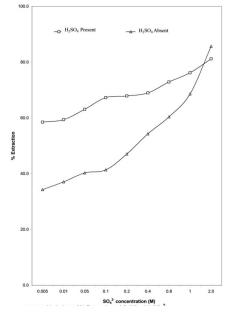


Fig. 15. Variation of % extraction of Cr (VI) with SO<sub>4</sub><sup>2-</sup> concentration for H<sub>2</sub>SP in CHCI<sub>3</sub>(in the presence and absence of H<sub>2</sub>SO<sub>4</sub>)

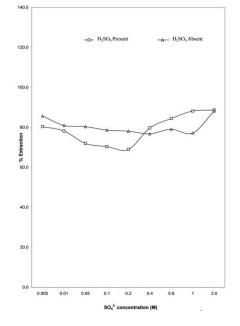


Fig. 16. Variation of % extraction of Cr (VI) with SO<sub>4</sub><sup>2-</sup> concentration for H<sub>2</sub>SP in CHCI<sub>3</sub>:BuOH(in the presence and absence of H<sub>2</sub>SO<sub>4</sub>)

been attributed to increase in formation of unextractable chloride and sulphate species of the metal at higher concentrations of these anions.

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A comparison of the masking effects of the halides on the extraction of Cr (VI) follows the following increasing order:

I'< Br'<CI

for both  $H_2Adp$  and  $H_2SP$  ligands. The trend is consistent with the decrease in electronegativity of the element and increase in ionic radius of the ion.

The effect of complexing agents such as,  $PO_4^{2^\circ}$ , acetate EDTA, oxalate and tartarate on the extraction of Cr (VI) ions appears to be fairly constant for both H<sub>2</sub>Adp and H<sub>2</sub>SP. The results obtained show that extractions of these metals are increasingly masked as anion concentration increase in the aqueous phase. This is consistent with results reported on Mo (VI) [21]. However higher percentages of 88 to 90% were obtained for Cr (VI) extractions using H<sub>2</sub>Adp compared to the results obtained for Mo (VI) in H<sub>2</sub>Adp (48 to 50%).

# **COMPETING INTERESTS**

Authors have declared that no competing interests exist.

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